

STEADY AND UNSTEADY 2D NUMERICAL SOLUTION OF GENERALIZED NEWTONIAN FLUIDS FLOW

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Introduction

● Mathematical model

- ▶ incompressible laminar viscous fluids flow
- ▶ generalized Newtonian fluids model
- ▶ stress tensor - Newtonian model
- ▶ viscosity - Newtonian - $\mu = \text{const.}$
- ▶ generalized Newtonian - power-law model

$$\mu = \mu(\dot{\gamma}) = \left(\sqrt{\text{tr}D^2} \right)^r$$

● Numerical model

- ▶ steady computation
- ▶ finite volume method
- ▶ artificial compressibility method
- ▶ multistage Runge-Kutta method
- ▶ unsteady computation
- ▶ dual-time stepping method

Mathematical Model

The system of 2D Navier-Stokes equations in conservative form

$$\tilde{R}W_t + F_x^c + G_y^c = F_x^v + G_y^v \quad \tilde{R} = \text{diag}(0, 1, 1) \quad (1)$$

where

$$W = \begin{pmatrix} p \\ u \\ v \end{pmatrix} \quad F^c = \begin{pmatrix} u \\ u^2 + p \\ uv \end{pmatrix} \quad G^c = \begin{pmatrix} v \\ uv \\ v^2 + p \end{pmatrix}$$

$$F^v = \begin{pmatrix} 0 \\ t_{xx} \\ t_{yx} \end{pmatrix} \quad G^v = \begin{pmatrix} 0 \\ t_{xy} \\ t_{yy} \end{pmatrix}$$

Mathematical Model - Stress Tensor

Newtonian model

$$\mathbf{T} = 2\mu\mathbf{D}$$

$$\mathbf{T} = \begin{pmatrix} t_{xx} & t_{xy} \\ t_{yx} & t_{yy} \end{pmatrix}$$

$$D_{ij} = \frac{1}{2} \left(\frac{\partial v_i}{\partial x_j} + \frac{\partial v_j}{\partial x_i} \right)$$

$$\mathbf{D} = \frac{1}{2} \begin{pmatrix} 2u_x & u_y + v_x \\ u_y + v_x & 2v_y \end{pmatrix}$$

Mathematical Model - Generalized Newtonian Fluids

$$T = 2\mu_e \mu D$$

Power-law model

$$\mu = \mu(\dot{\gamma}) = \mu_e \left(\sqrt{\text{tr}D^2} \right)^r$$

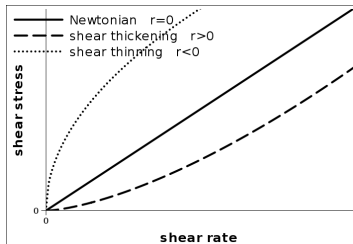
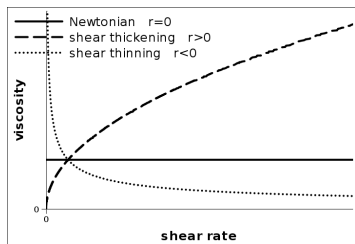
μ_e - Newtonian viscosity

r - power-law index

$r = 0$ - Newtonian fluids flow

$r > 0$ - shear thickening fluids flow

$r < 0$ - shear thinning fluids flow



Steady Numerical Solution

Eq. (1) - steady state solution

$$\tilde{R}W_t + F_x^c + G_y^c = \frac{1}{\text{Re}}(F_x^v + G_y^v), \quad \tilde{R}_\beta = \text{diag}(0, 1, 1)$$

Artificial compressibility method

$$\tilde{R}_\beta W_t + F_x^c + G_y^c = \frac{1}{\text{Re}}(F_x^v + G_y^v), \quad \tilde{R}_\beta = \text{diag}\left(\frac{1}{\beta^2}, 1, 1\right), \quad \text{Re} = \frac{UL}{\mu_\epsilon}$$

$$W = \begin{pmatrix} p \\ u \\ v \end{pmatrix}, \quad F^c = \begin{pmatrix} u \\ u^2 + p \\ uv \end{pmatrix}, \quad G^c = \begin{pmatrix} v \\ uv \\ v^2 + p \end{pmatrix}$$

$$F^v = \begin{pmatrix} 0 \\ 2\mu(\dot{\gamma})u_x \\ \mu(\dot{\gamma})(v_x + u_y) \end{pmatrix}, \quad G^v = \begin{pmatrix} 0 \\ \mu(\dot{\gamma})(u_y + v_x) \\ 2\mu(\dot{\gamma})v_y \end{pmatrix}$$

Multistage Runge-Kutta Method

$$W_i^n = W_i^{(0)}$$

$$W_i^{(s)} = W_i^{(0)} - \alpha_s \Delta t \mathcal{R}(W)_i^{(s-1)}$$

$$W_i^{n+1} = W_i^{(m)} \quad s = 1, \dots, m$$

$$m = 3, \quad \alpha_1 = \alpha_2 = 0.5, \quad \alpha_3 = 1.$$

steady residual

$$\mathcal{R}(W)_i = \frac{1}{\mu_i} \sum_{k=1}^4 \left[\left(\bar{F}_k^c - \frac{1}{\text{Re}} \bar{F}_k^v \right) \Delta y_k - \left(\bar{G}_k^c - \frac{1}{\text{Re}} \bar{G}_k^v \right) \Delta x_k \right]$$

Numerical Fluxes

$\overline{F}_k^c, \overline{G}_k^c$... inviscid numerical fluxes

$$\overline{F}_k^c = F_k^c \left(\frac{W_i + W_k}{2} \right) \quad \overline{G}_k^c = G_k^c \left(\frac{W_i + W_k}{2} \right)$$

dissipative numerical fluxes $\overline{F}_k^v, \overline{G}_k^v$ are computed using dual volume cells (Green formula)

numerical approximations of the velocity derivatives

$$\overline{u}_x = \frac{1}{\mu_k} \sum_{m=1}^4 u_m \Delta y_m \quad \overline{u}_y = -\frac{1}{\mu_k} \sum_{m=1}^4 u_m \Delta x_m$$

Time Step and Convergence (Runge-Kutta Scheme)

The condition of stability at regular orthogonal grid

$$\Delta t = \min_{i,k} \frac{\text{CFL} \mu_i}{\rho_A \Delta y_k + \rho_B \Delta x_k + \frac{2}{\text{Re}} \mu(\dot{\gamma}) \left(\frac{(\Delta x_k)^2 + (\Delta y_k)^2}{\mu_i} \right)}$$

Convergence to steady state is checked by behavior of steady residual in the space L^2

$$\text{Res } W^n = \sqrt{\frac{1}{\text{num}} \sum_i \left(\frac{W_i^{n+1} - W_i^n}{\Delta t} \right)^2}$$

num - number of the finite volume cells

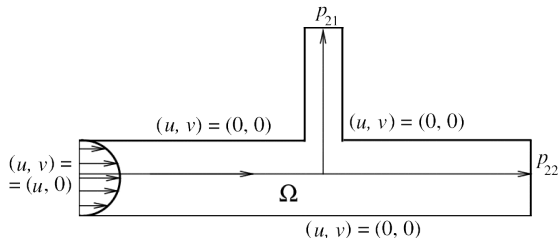
The decadic logarithm of $\|\text{Res}(W)^n\|_{L^2}$ is plotted in graphs presenting convergence history of simulation.

Boundary Conditions

Eq. (1) solved in the domain Ω

$$\tilde{R}W_t + F_x^c + G_y^c = F_x^v + G_y^v \quad \tilde{R} = \text{diag}(0, 1, 1)$$

- inlet conditions
 - Dirichlet BC
 - parabolic profile
- outlet conditions
 - $p = p_{21}, p_{22}$,
- wall conditions
 - $(u, v)^T = (0, 0)^T$
- other values of W
 - Neumann BC



Unsteady Numerical Solution

Dual-time stepping method

$$\tilde{R}_\beta W_\tau + \tilde{R} W_t + F_x^c + G_y^c = F_x^v + G_y^v$$

$$\tilde{R}_\beta = \text{diag}\left(\frac{1}{\beta^2}, 1, 1\right) \quad \tilde{R} = \text{diag}(0, 1, 1)$$

Three point backward formula

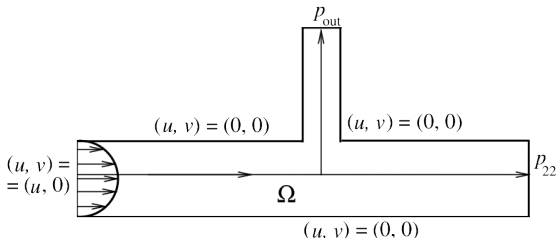
$$\tilde{R}_\beta \frac{W^{l+1} - W^l}{\Delta\tau} = -\tilde{R} \frac{3W^{l+1} - 4W^n + W^{n-1}}{2\Delta t} - \text{Res}(W)^l = -\overline{\text{Res}(W)}^{l+1}$$

l - dual time, n - physical time

$l \rightarrow \infty \Rightarrow n \rightarrow (n+1)$

Unsteady Boundary Condition

- inlet conditions
 - Dirichlet BC
 - parabolic profile
- outlet conditions
 - $p = p_{22}$,
- wall conditions
 - $(u, v)^T = (0, 0)^T$
- other values of W
 - Neumann BC



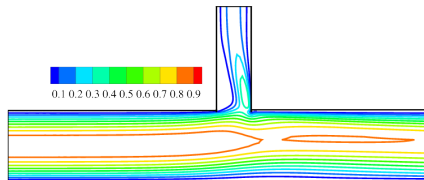
$$p_{out} = \frac{1}{4} \left(1 + \frac{1}{2} \sin(\omega t) \right)$$

ω - angular velocity, $\omega = 2\pi f$

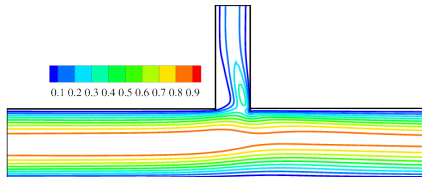
f - frequency

Steady Numerical Results - $Re = 400$

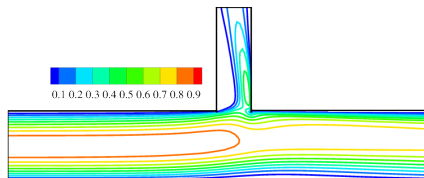
Newtonian fluids ($r = 0$)



Shear thickening Non-Newtonian fluids ($r = 0.5$)

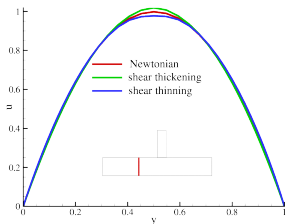
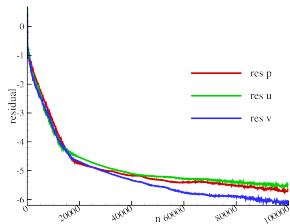


Shear thinning Non-Newtonian fluids ($r = -0.5$)

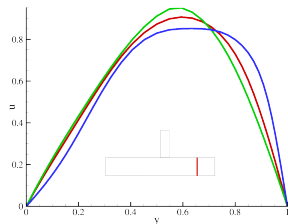
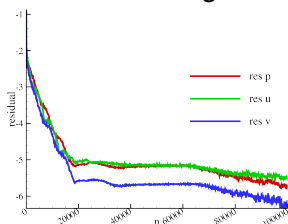


Steady Numerical Results

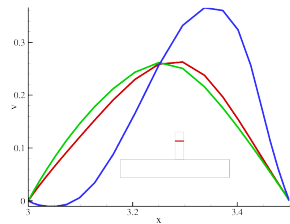
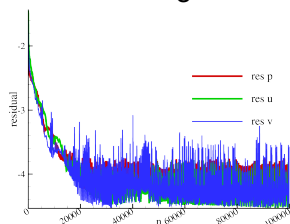
Newtonian fluids



Shear thickening fluids

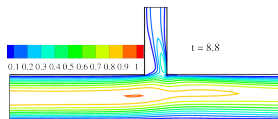
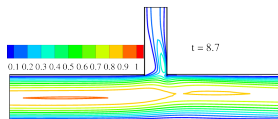
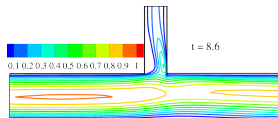
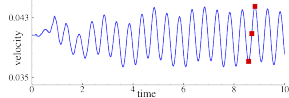


Shear thinning fluids

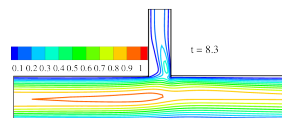
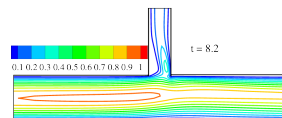
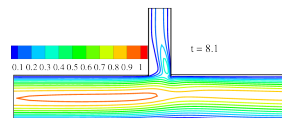
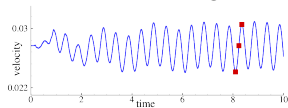


Unsteady Numerical Results, Artificial Compressibility Method, frequency $f = 2$

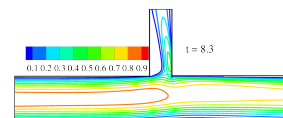
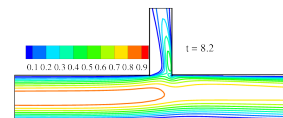
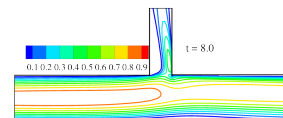
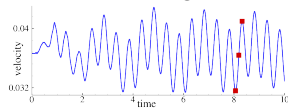
Newtonian



Shear thickening

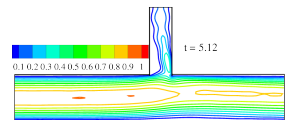
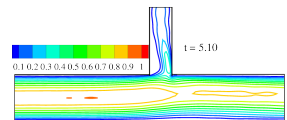
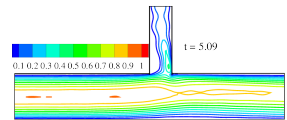
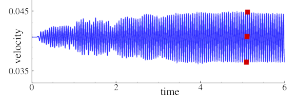


Shear thinning

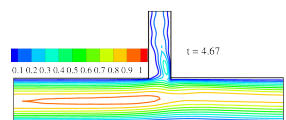
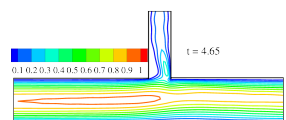
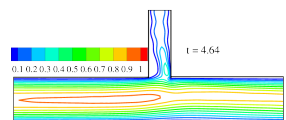
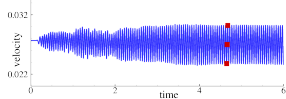


Unsteady Numerical Results, Artificial Compressibility Method, frequency $f = 20$

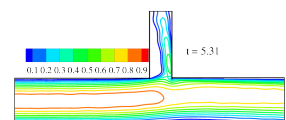
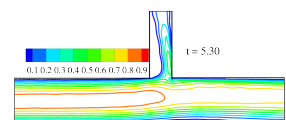
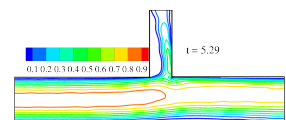
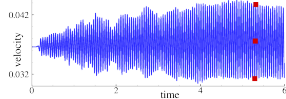
Newtonian



Shear thickening

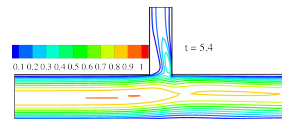
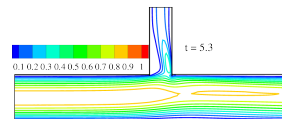
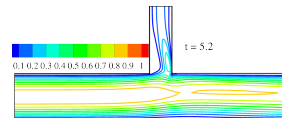
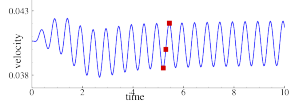


Shear thinning

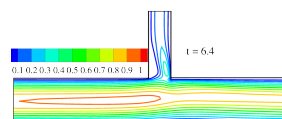
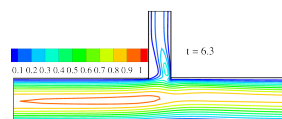
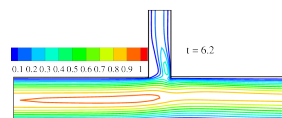
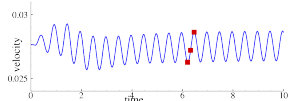


Unsteady Numerical Results, Dual-Time Stepping Method, frequency $f = 2$

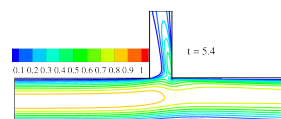
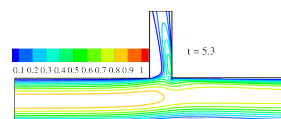
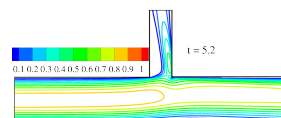
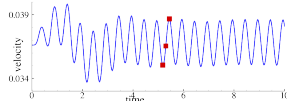
Newtonian



Shear thickening

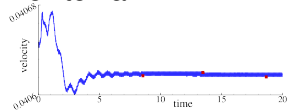


Shear thinning

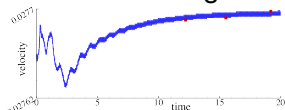


Unsteady Numerical Results, Dual-Time Stepping Method, frequency $f = 20$

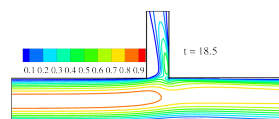
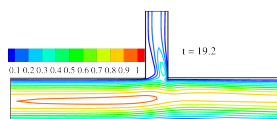
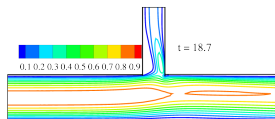
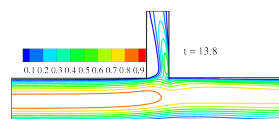
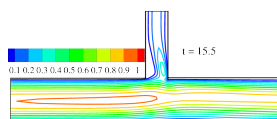
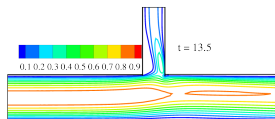
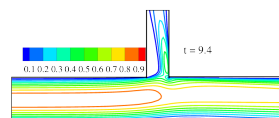
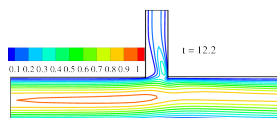
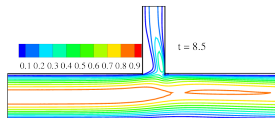
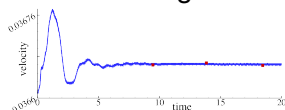
Newtonian



Shear thickening



Shear thinning



Conclusion

- Mathematical model for generalized Newtonian fluids (Newtonian and non-Newtonian shear thickening and shear thinning fluids)
- Numerical method for steady and unsteady simulations
- Finite volume method, Runge-Kutta scheme
- Unsteady computations - artificial compressibility method and dual time-stepping method